# Lanthanide Oxide Doped Titanium Dioxide Photocatalysts: Effective Photocatalysts for the Enhanced Degradation of Salicylic Acid and t-Cinnamic Acid

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**The photocatalytic degradation of salicylic acid and** *t***-cinnamic acid has been investigated in aqueous suspensions of lanthanide oxide doped TiO2 photocatalysts. Complete mineralization has been achieved in the case of lanthanide oxide doped TiO2 photocatalysts in total contrast to the formation of intermediates in case of non**modified TiO<sub>2</sub>. The equilibrium dark adsorption of salicylic acid **and** *t***-cinnamic acid is ca. three times and two times higher, respectively, on the lanthanide oxide modified catalysts as compared to the nonmodified TiO2 catalyst. The adsorption isotherms were analyzed in terms of the Langmuir theory and a good fit was obtained. The enhanced degradation is attributed to the formation of the Lewis acid–base complex between the lanthanide ion and the substrates at the photocatalyst surface. The concentration of the** organic acids at the composite  $Ln<sub>2</sub>O<sub>3</sub>/TiO<sub>2</sub>$  photocatalysts could **provide a means for the enhanced activity.** © 2001 Elsevier Science

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## **INTRODUCTION**

The study of light-induced reactions catalyzed by semiconductors has been widely studied particularly during the past decade (1–5). A wide range of organic compounds such as phenols, aromatic carboxylic acids, dyes, surfactants, and pesticides have been successfully mineralized (6–10). Photocatalysis has also proven useful in the reductive deposition of heavy and noble metal ions like  $Pt^{4+}$ ,  $Au^{3+}$ ,  $Rh^{3+}$ ,  $Cr^{3+}$ , etc. from aqueous solutions to surfaces (11–14). Among the several semiconductors employed for the degradation of organic compounds,  $TiO<sub>2</sub>$  has proven to be a versatile catalyst for detoxification of organic pollutants. The excellent stability coupled with low cost has made  $TiO<sub>2</sub>$  a benchmark catalyst in semiconductor photocatalysis. In order to effectively compete with *e*−/*h*<sup>+</sup> recombination and trap effectively the conduction band electrons or the valence band holes, the respective electron acceptor or donor should be confined to the semiconductor surface. Several methods have been suggested to control the interfacial electron transfer at the semiconductor–electrolyte interface. These include encapsulation of electron acceptors on receptor functionalized semiconductors, (15) immobilization of semiconductor photocatalysts in redox functionalized polymers, (16) and electrostatic association of electron acceptors at the semiconductor surface (17).

Another method to improve the degradation is to preconcentrate the organic substrate at the semiconductor surface in order to effectively trap the respective reactive radicals. Concentration of the organic pollutant at the semiconductor surface has been achieved by selective doping of the semiconductor, (18) surface modification of the photocatalyst with chelating agents, (19) and surface modification of the catalyst with electron acceptors groups (20).

Lanthanide ions are known for their ability to form complexes with various Lewis bases (e.g., acids, amines, aldehydes, alcohols, thiols, etc.) in the interaction of these functional groups with the *f* orbitals of the lanthanides (21). Thus, incorporation of lanthanide ions in a  $TiO<sub>2</sub>$  matrix could provide a means to concentrate the organic pollutant at the semiconductor surface. The sol–gel method enables the synthesis of a high surface area  $TiO<sub>2</sub>$  particle (22). Here we wish to report on the degradation of salicylic acid and  $t$ -cinnamic acid on lanthanide oxide doped  $TiO<sub>2</sub>$  particles. The choice of salicylic acid as the substrate was based on the fact that it is well documented that aromatic carboxylic acids such as salicylic acid have great affinity for aqueous  $Ti(IV)$  and a strong tendency to chemisorb (24–26). Thus, it is important to assess if the activity of lanthanide oxide doped  $TiO<sub>2</sub>$  extends to the degradation of salicylic acid.

The photocatalytic degradation of salicylic acid has been the subject of numerous investigations. Matthews has studied the kinetics and the photocatalytic oxidation of salicylic acid on  $TiO<sub>2</sub>$  thin films, and a reaction mechanism involving peroxyhydroxycyclohexadienyl- and



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mucondialdehyde-type compounds as intermediates was proposed (27–31). Titanium dioxide aerogels, cryogels, and nanofibrils were also evaluated for the degradation of salicylic acid in aqueous environments (32–34).

## **EXPERIMENTAL**

The nonmodified  $TiO<sub>2</sub>$ , europium (Eu<sup>3+</sup>), praseodymium  $(Pr<sup>3+</sup>)$ , and ytterbium  $(Yb<sup>3+</sup>)$  doped TiO<sub>2</sub> were prepared as shown in Scheme 1. The preparation of these catalysts has been reported previously (18). The molar ratio of Ti(IV) to  $Eu(III)$ ,  $Pr(III)$ , or  $Yb(III)$  is usually 100, but a catalyst having a molar ratio of Ti(IV) to Eu(III) corresponding to  $Ti/Eu = 20$  was also prepared. The X-ray diffractograms of the calcined samples were recorded using a Philips PW 1050 powder diffractometer. The diffraction patterns were recorded at room temperature using a Ni-filtered Cu*K* $\alpha$  radiation ( $\lambda = 1.5418$  Å) for the samples. Surface area measurements were measured by nitrogen adsorption at−196◦C by the dynamic BET method using a Micromeritics II 2370 surface area analyzer. The transmission electron micrographs (TEM) of the samples were recorded using a JEOL, JEM-100 CX, electron microscope, operating at an accelerating voltage of 80 kV. X-ray photoelectron spectroscopy (XPS) analyses were performed with an AXIS-HS Kratos instrument using a monochromatized  $Al(K\alpha)$ source  $(hv = 1486.6 \text{ eV})$ . A flood gun was used to neutral-



**SCHEME 1.** Preparation of the lanthanide oxide doped  $TiO<sub>2</sub>$  catalysts.

ize the sample surface, while the C (1s) line was used for a final energy scale calibration.

Adsorption of the organic substrate onto the catalysts was examined by stirring 2.5 mg of the catalyst in 2.5 ml of appropriate concentrations of the substrates in the dark. After equilibration for 1 h, the catalyst was filtered using a  $0.05$ - $\mu$ m polycarbonate filter and the concentration of the organic substrate was determined spectroscopically. The concentrations of salicylic acid and *t*-cinnamic acid before and after adsorption were measured from their absorption maximum at  $\lambda = 295$  nm and  $\lambda = 272$  nm, respectively. Photochemical degradation of salicylic acid and *t*-cinnamic acid was examined. The aqueous solution of the pollutant (2.5 mL),  $2.4 \times 10^{-4}$  M (salicylic acid) or  $2.2 \times 10^{-5}$  M (*t*-cinnamic acid), and 2.0–2.4 mg of the respective photocatalysts were placed in a quartz cuvette (5-mL capacity). The suspension was irradiated with a 200-W Xe(Hg) lamp (Oriel) equipped with an CuSO4 solution to filter IR radiation. The flux of photons entering the reactor was ∼6 × 10−<sup>6</sup> einsteins/s in the 300- to 400-nm-wavelength range. A Pyrex filter was used to filter the light of wavelengths less than 300 nm that would cause direct photodegradation of the organic substrates. During irradiation, the suspension was stirred continuously and purged with oxygen. Oxygen bubbling throughout the experiment maintained a dissolved oxygen concentration of  $\sim$ 1 × 10<sup>-4</sup> mol dm<sup>-3</sup>. After irradiation, the suspension was filtered to remove the catalyst and the solution was analyzed spectroscopically (Uvikon-860 Kontron Spectrophotometer) and by gas chromatography–mass spectrometry/Fourier transform infrared spectroscopy (GC–MS/FTIR).

The light absorbed by the particles was determined by placing a radiometer at the back side of the quartz cuvette which contains the organic substrate solution alone or the same solution containing 2.0–2.4 mg of the modified  $TiO<sub>2</sub>$ particles. The difference between the two recorded values was assumed to correspond to the absorbed light intensity. Since light scattering by the particles is neglected, the absorbed light intensities could be considered as upper limits.

#### *DOC Analyses*

The analysis of dissolved organic carbon (DOC) was carried out using a Dohrmann DC-190 total organic carbon (TOC) analyzer ( $T = 680^{\circ}$ C) from Rosemount Analytical. The organic components were oxidized in an oxygen atmosphere at a platinum/alumina contact. The amount of carbon dioxide formed was measured using a nondispersive IR detector. The TOC content was analyzed in this manner and the inorganic carbon content was subtracted from this value. The latter is obtained by treating the samples with concentrated phosphoric acid. The calibration was performed using salicylic acid, oxalic acid, and potassium hydrophthalate (KHP). All calibration samples could be

fitted with a linear calibration curve. The samples were injected three consecutive times (injection volume 50  $\mu$ l) and the average values were reported.

## *GC–MS/FTIR Analysis*

For the quantitative and qualitative analysis of the reaction products generated during the photolysis experiments, the samples  $(2 \mu l)$  were injected into a GC (HP 5971A) MSD, mass selective detector) coupled with a HP 5965B 1D (infrared detector). A HP-INNOWAX capillary column (cross-linked polyethylene glycol) was employed. All reaction products were identified by a combination of MS and FTIR spectroscopy in comparison with analytical databases.

### **RESULTS AND DISCUSSION**

Table 1 shows the physical properties of the  $T_1O_2$  catalysts prepared in the present study. The X-ray diffractograms of the samples reveal that in the case of the nonmodified  $TiO<sub>2</sub>$ , the anatase phase is the major constituent of the photocatalyst (80%) accompanied by a rutile phase (20%). In the case of  $Eu_2O_3/TiO_2$  and  $Yb_2O_3/TiO_2$  the anatase phase is predominant ( $>95\%$ ), while in the case of Pr<sub>2</sub>O<sub>3</sub>/TiO<sub>2</sub> catalyst, the X-ray diffractogram reveals the presence of only the anatase phase. XPS measurements reveal that the lanthanide does exist in the resulting  $TiO<sub>2</sub>$  photocatalysts as oxides,  $Ln<sub>2</sub>O<sub>3</sub>$ . Lanthanide concentrations were evaluated from their 3d and 4d lines. The europium-doped TiO<sub>2</sub> photocatalysts, having a molar ratio of Ti/Eu = 20 and Ti/Eu = 100, show a characteristic band at 1134.7 eV due to the Eu<sup>3+</sup> ion. The band characteristic of  $Ti^{4+}$  appears at 458.6 eV. The ratio of atomic concentration of Ti/Eu in the doped  $Eu_2O_3/TiO_2$ (starting molar composition Ti/Eu = 20) at the surface was evaluated to be  $20 \pm 2$ , in full agreement with the molar ratio of the ions used in the preparation of the photocatalyst prior to the calcination. However, for the catalyst  $Eu_2O_3/TiO_2$  (starting molar composition Ti/Eu = 100), the ratio of the Ti/Eu at the surface was evaluated to be  $\sim$ 40 ± 4 from XPS studies. Thus,









**FIG. 1.** Absorption spectra of an aqueous solution of salicylic acid  $(2.4 \times 10^{-4}$  M) (a) before irradiation, (b) after 30 min of irradiation, (c) after 45 min of irradiation, and (d) after 60 min of irradiation in the presence of the  $Eu_2O_3/TiO_2$  catalyst (Ti/Eu = 20) (2.4 mg in 2.5 ml of the solution).

there seems to be an enrichment of  $Eu^{3+}$  ion at the surface due to segregation of  $Eu<sub>2</sub>O<sub>3</sub>$  to the surface after calcination. An additional Eu signal around 1125 eV was observed in the  $Eu_2O_3/TiO_2$  samples, associated with the reduced form of the europium. This is believed to be induced by the X-ray beam during the measurement. The magnitude of this signal ranged from 20 to 35% of the total europium signal for the  $Eu_2O_3/TiO_2$ , Ti/Eu = 20, and Ti/Eu = 100 samples, respectively. This was in fact inspected as a function of X-ray irradiation time, and a proportional trend was observed. Due to the low concentration of the lanthanide ions, low irradiation exposures did not yield satisfactory signal-to-noise ratios. The XPS analysis of the  $Yb_2O_3/TiO_2$  catalyst reveals a signal at approximately 185.5 eV due to  $Yb^{3+}$  (4d) with a Ti/Yb =  $200 \pm 50$ . In the case of the Pr<sub>2</sub>O<sub>3</sub>/TiO<sub>2</sub> catalyst, the signal due to  $Pr^{3+}$  (3d) appears at 933.5 eV. The  $Yb_2O_3/TiO_2$  and  $Pr_2O_3/TiO_2$  catalysts show a lower surface concentration of  $\text{Ln}^{3+}$  ions as compared to the concentration used in the preparation of the gel.

The photodegradation of salicylic acid and *t*-cinnamic acid by  $Eu_2O_3/TiO_2$  was examined and compared with the nonmodified  $TiO<sub>2</sub>$ . Figure 1 shows the absorbance spectra of salicylic acid solution at time intervals of irradiation with the  $Eu_2O_3/TiO_2$  catalyst (Ti/Eu = 20). A substantial decrease in the absorbance of the substrate at all wavelengths is observed indicating its degradation. The substrate is completely degraded in the presence of the  $Eu_2O_3/TiO_2$  catalyst. The absorbance spectra of salicylic acid reacted over  $Eu_2O_3/TiO_2$  (Ti/Eu = 100),  $Pr_2O_3/TiO_2$ , and  $Yb_2O_3/TiO_2$  catalysts after 60 min of irradiation were similar to of the  $Eu_2O_3/TiO_2$  catalyst (Ti/Eu = 20), indicating its mineralization. In contrast, a smaller decrease (∼54%) in the absorbance of the substrate is observed over the nonmodified  $TiO<sub>2</sub>$  catalyst after 60 min of irradiation (not shown). The photodegradation of salicylic acid by the lanthanide oxide doped  $TiO<sub>2</sub>$  catalysts leads



**FIG. 2.** Degradation of salicylic acid  $(2.4 \times 10^{-4} \text{ M})$  over (a) Eu<sub>2</sub>O<sub>3</sub>/ TiO<sub>2</sub> (Ti/Eu = 100) catalyst, (b)  $Pr_2O_3/TiO_2$  catalyst, (c)  $Yb_2O_3/TiO_2$ catalyst, and (d) nonmodified  $TiO<sub>2</sub>$  catalyst. In all experiments, 2.2–2.5 mg of the catalyst in 2.5 ml of the solution was used.

to complete mineralization as observed by GC–MS results (see later). The superior performance of the lanthanide oxide doped catalysts is clearly evident. Figure 2 shows the results obtained from the degradation of salicylic acid over the various  $TiO<sub>2</sub>$  catalysts. After 60 min of irradiation, 84, 95, 90, and 93% of salicylic acid are degraded by the  $Eu_2O_3/TiO_2$  (Ti/Eu = 20),  $Eu_2O_3/TiO_2$  (Ti/Eu = 100),  $Pr_2O_3/TiO_2$ , and  $Yb_2O_3/TiO_2$  catalysts as compared to 54% by the nonmodified  $TiO<sub>2</sub>$  photocatalyst.

To account for the enhanced photocatalytic activity of the lanthanide oxide doped catalysts as compared to the nonmodified  $TiO<sub>2</sub>$ , the adsorption of salicylic acid to the  $Eu_2O_3/TiO_2$  (Ti/Eu = 20) catalyst and nonmodified TiO<sub>2</sub> catalyst was examined. Figure 3 shows the adsorption isotherm of salicylic acid on  $Eu_2O_3/TiO_2$  (Ti/Eu = 20). The amount of salicylic acid adsorbed onto the photocatalyst increases as the bulk concentration of the substrate is increased and then reaches a saturation value that represents the maximum loading of the substrate. For  $Eu_2O_3/TiO_2$ (Ti/Eu = 20), the saturation value of  $2.2 \times 10^{-6}$  mol g<sup>-1</sup> of salicylic acid on the catalyst is obtained at a bulk concentration of  $2.65 \times 10^{-3}$  M. The presence of an adsorption maximum indicates that a simple Langmuir equation, which assumes the presence of only one type of surface site, should be applicable in the present study. The adsorption isotherm was analyzed in terms of the Langmuir theory(35). A linear relationship in agreement with the Langmuir theory between  $[C]_{eq}/C_{ads}$  as a function of  $[C]_{eq}$  was obtained (not shown);  $[C]_{\text{eq}}$  represents the equilibrium bulk concentration of salicylic acid and *C*ads is the amount (in moles) of salicylic acid adsorbed onto the photocatalysts. Thus, a simple Langmuir equation did fit our data satisfactorily. This is in contrast to the results obtained by Tunesi and Anderson (24) and Regazzoni *et al.* (26). Tunesi and Anderson (24) reported a Freundlich isotherm to be a representation for the adsorption of salicylic acid and 3-chlorosalicylic acid over  $TiO<sub>2</sub>$  catalysts. They did not observe any adsorption maximum which may mean that they have not saturated the surface sites, or possibly have several types of sites or have a continuum of sites. A multisite surface complex model was proposed by Regazzoni *et al.* (26) to explain the adsorption of salicylic acid over the  $TiO<sub>2</sub>$  catalyst (Degussa P-25). Our results are in agreement with those reported by Cunningham and Al-Sayyed (36). This suggests that in the present study, the  $\text{Ln}_2\text{O}_3/\text{TiO}_2$  composite photocatalysts consist of lanthanide oxide particles uniformly dispersed on the surface and in the bulk giving rise to  $TiO<sub>2</sub>$  surface hydroxyl groups that have only one degree of acidity. Thus, the surface with respect to the adsorption process is homogeneous accounting for the good fit to the one-site Langmuir adsorption isotherm. The derived adsorption constant on Eu<sub>2</sub>O<sub>3</sub>/TiO<sub>2</sub> (Ti/Eu = 20) is  $K_{ads} = 4.08 \times 10^3$  M<sup>-1</sup>. From Fig. 4 for the nonmodified  $TiO<sub>2</sub>$  catalyst, the saturation



**FIG. 3.** Adsorption isotherm of salicylic acid over  $Eu_2O_3/TiO_2$  catalyst  $(Ti/Eu = 20)$ .



**FIG. 4.** Adsorption isotherm of salicylic acid over nonmodified TiO<sub>2</sub> catalyst.

value of  $1.33 \times 10^{-6}$  mol g<sup>-1</sup> on the catalyst is obtained at a bulk concentration of  $3.05 \times 10^{-3}$  M. The derived adsorption constant on nonmodified TiO<sub>2</sub> is  $K_{ads} = 1.25 \times 10^3 \,\mathrm{M}^{-1}$ . Similarly, the adsorption constants of salicylic acid were determined to be  $K_{\text{ads}} = 3.6 \times 10^3 \text{ M}^{-1}$  for Eu<sub>2</sub>O<sub>3</sub>/TiO<sub>2</sub>  $(Ti/Eu = 100)$   $K_{ads} = 3.0 \times 10^3$  M<sup>-1</sup> for Pr<sub>2</sub>O<sub>3</sub>/TiO<sub>2</sub>, and  $K_{\text{ads}} = 2.8 \times 10^3 \text{ M}^{-1}$  for Yb<sub>2</sub>O<sub>3</sub>/TiO<sub>2</sub>. The enhanced adsorption constant is attributed to the formation of Lewis acid–base complexes between the lanthanide ions in the modified  $TiO<sub>2</sub>$  and the carboxylic acid residue of the substrate. The concentration of the substrate at the photocatalytic surface could then provide the mechanism for the enhanced mineralization of salicylic acid by the modified photocatalysts.

The concentrations of the solutions after irradiation were also monitored by GC–MS analyses. Table 2 shows the results obtained from the GC–MS study for the degradation of salicylic acid by the lanthanide oxide doped catalysts. The GC–MS results clearly reveal the superior performance of the lanthanide oxide doped catalysts. For example, from Table 2 we can see that after 30 min of irradiation, the concentration of salicylic acid is 11.2 ppm with the  $Eu_2O_3/TiO_2$ catalyst (Ti/Eu = 100), whereas it is 25.5 ppm with the nonmodified catalyst. After 60 min of irradiation, complete mineralization of salicylic acid is achieved by the lanthanide oxide doped catalysts while the concentration of salicylic acid is 17.4 ppm with the nonmodified catalyst. The spectroscopic assay of the degradation rates of salicylic acid coincides with the results obtained from the GC–MS analysis of the irradiated samples. Figure 5 shows the results obtained from the GC–MS analysis and the spectroscopic analysis for the  $Eu_2O_3/TiO_2$  catalyst (Ti/Eu = 100).

It is worthwhile to also compare the rate of photodegradation of salicylic acid by  $Eu_2O_3/TiO_2$  catalysts that include different amounts of europium oxide. The rate of degradation of salicylic acid was found to be twice as fast in the presence of the  $Eu_2O_3/TiO_2$  catalyst (Ti/Eu = 100)  $(k = 2.2 \text{ s}^{-1})$  as compared to the photocatalyst containing Ti/Eu = 20 ( $k = 0.9$  s<sup>-1</sup>). The rate of degradation was estimated from the initial decrease in the concentration of salicylic acid assuming first-order kinetics. The fact that the  $Eu_2O_3/TiO_2$  catalyst (Ti/Eu = 20) is less efficient implies that the improved adsorption of the pollutants to the europium oxide doped photocatalysts is not the sole operative mechanism that controls the activity of the photocatalysts since the adsorption of salicylic acid is higher on the Ti/Eu catalyst (Ti/Eu = 20) ( $K_{ads} = 4.08 \times 10^3$  M<sup>-1</sup>) compared to the Eu<sub>2</sub>O<sub>3</sub>/TiO<sub>2</sub> catalyst (Ti/Eu = 100) ( $K_{ads} = 3.6 \times$  $10^3$  M<sup>-1</sup>). The Eu<sub>2</sub>O<sub>3</sub>/TiO<sub>2</sub> catalyst (Ti/Eu = 20) absorbs ca. 20% more incident light as compared to the  $Ti/Eu = 100$ catalyst (not shown). Thus the lower activity exhibited by

TABLE	
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**GC–MS Results Obtained for the Degradation of Salicylic Acid over Lanthanide Oxide Doped TiO2 Catalysts and Nonmodified TiO2 Catalyst**



*<sup>a</sup>* Not determined.





**FIG. 5.** Degradation of salicylic acid  $(2.4 \times 10^{-4} \text{ M})$  over Eu<sub>2</sub>O<sub>3</sub>/TiO<sub>2</sub>  $(Ti/Eu = 100)$  catalyst (a) analyzed by GC–MS, (b) analyzed spectroscopically. In all experiments, 2.2–2.5 mg of the catalyst in 2.5 ml of the solution was used.

the  $Eu_2O_3/TiO_2$  catalyst (Ti/Eu = 20) can be attributed to the light filtering effect since europium oxide absorbs part of the incident light. The onset of absorption for  $Eu<sub>2</sub>O<sub>3</sub>$  is ∼320 nm.

In order to test the generality of the enhanced activity of the lanthanide oxide doped catalysts, the degradation of another aromatic carboxylic acid compound, namely, *t*cinnamic acid, was evaluated. Figure 6 shows the absorp-



**FIG. 6.** Absorption spectra of an aqueous solution of *t*-cinnamic acid  $(2.2 \times 10^{-5}$  M) (a) before irradiation, (b) after 45 min of irradiation in the presence of the  $Eu_2O_3/TiO_2$  (Ti/Eu = 100) catalyst, (c) after 45 min of irradiation in the presence of the  $Pr_2O_3/TiO_2$  (Ti/Pr = 100) catalyst, (d) after 45 min of irradiation in the presence of the  $Yb_2O_3/TiO_2$  (Ti/Yb = 100) catalyst, and (e) after 45 min of irradiation in the presence of the nonmodified  $TiO<sub>2</sub>$  catalyst. In all experiments, 2.2–2.5 mg of the catalyst in 2.5 ml of the solution was used.

**FIG. 7.** Degradation of *t*-cinnamic acid  $(2.2 \times 10^{-5} \text{ M})$  over Ln<sub>2</sub>O<sub>3</sub>/  $TiO<sub>2</sub>$  catalysts and nonmodified  $TiO<sub>2</sub>$  catalyst.

tion spectra of *t*-cinnamic acid solution at time intervals of irradiation with the lanthanide oxide doped catalysts and the nonmodified  $TiO<sub>2</sub>$  catalyst. It is evident that the substrate is degraded at an impressive rate in the presence of the lanthanide oxide doped catalysts as compared to the nonmodified TiO<sub>2</sub> catalyst. *t*-cinnamic acid is completely degraded in the presence of the lanthanide oxide doped catalysts after 60 min of irradiation whereas only 45% is degraded by the nonmodified  $TiO<sub>2</sub>$  catalyst (Fig. 7). Table 3 summarizes the results obtained from the photodegradation of salicylic acid and *t*-cinnamic acid over nonmodified  $TiO<sub>2</sub>$  and  $Ln<sub>2</sub>O<sub>3</sub>/TiO<sub>2</sub>$  photocatalysts. Table 4 shows the results obtained from the GC–MS analyses. The GC–MS results indicate that *t*-cinnamic acid is completely degraded

## **TABLE 3**

**Amount of Salicylic Acid and** *t***-Cinnamic Acid Degraded (Analyzed Spectroscopically) after 60 and 45 min of Irradiation over** Lanthanide Oxide Doped TiO<sub>2</sub> Catalysts and Nonmodified TiO<sub>2</sub> **Catalyst, Respectively**



*<sup>a</sup>* Formation of intermediates.

#### **TABLE 4**

	TiO <sub>2</sub>		$Eu_2O_3/TiO_2$ $(Ti/Eu = 100)$		$Pr_2O_3/T_1O_2$		$Yb_2O_3/TiO_2$	
Time (min)	GC-FID/MS (ppm)	DOC (ppm)	GC-FID/MS (ppm)	<b>DOC</b> (ppm)	GC-FID/MS (ppm)	DOC (ppm)	GC-FID/MS (ppm)	DOC (ppm)
$\mathbf{0}$	58.0	58.0	58.0	58.0	58.0	58.0	58.0	58.0
15	51.2	56.5	24.0	40.2	18.7	35.0	28.5	41.5
30	38.4	51.4	0.0	18.7	0.0	4.9	5.6	20.3
45	31.6	45.0	0.0	9.5	0.0	$1.1\,$	0.0	12.7

**GC–MS Results Obtained for the Degradation of** *t***-Cinnamic Acid over Lanthanide Oxide Doped TiO2 Catalysts and Nonmodified TiO2 Catalyst**

in the presence of  $Eu_2O_3/TiO_2$  and  $Pr_2O_3/TiO_2$  catalysts after 30 min of irradiation, whereas only 34% is degraded over the nonmodified  $TiO<sub>2</sub>$  catalyst. After 45 min of irradiation, complete degradation of *t*-cinnamic acid is achieved by  $\text{Ln}_2\text{O}_3/\text{TiO}_2$  photocatalysts, whereas 45% is degraded by the nonmodified  $TiO<sub>2</sub>$  photocatalyst. The GC–MS results indicate that in the case of the nonmodified  $TiO<sub>2</sub>$  catalyst at least 20 intermediates were detected. Some of the intermediates that were detected were phenol, oxalic acid, salicylic acid, and benzoic acid. For  $\text{Ln}_2\text{O}_3/\text{TiO}_2$  photocatalysts, oxalic acid was detected as the only intermediate. After 45 min of irradiation, the concentration of oxalic acid was found to be 2.7 ppm for  $Eu_2O_3/TiO_2$ , 1.0 ppm for  $Yb_2O_3/TiO_2$ , and 2.5 ppm for  $Pr_2O_3/TiO_2$ .

The adsorption constants of *t*-cinnamic acid over the lanthanide oxide doped catalysts and the nonmodified  $TiO<sub>2</sub>$ catalyst were evaluated. The adsorption constants were determined to be  $K_{ads} = 6.0 \times 10^2$  M<sup>-1</sup> for nonmodified TiO<sub>2</sub>,  $K_{\text{ads}} = 2.0 \times 10^3 \text{ M}^{-1}$  for Eu<sub>2</sub>O<sub>3</sub>/TiO<sub>2</sub> (Ti/Eu = 100),  $K_{\text{ads}} = 1.5 \times 10^3 \text{ M}^{-1}$  for Pr<sub>2</sub>O<sub>3</sub>/TiO<sub>2</sub>, and  $K_{\text{ads}} = 1.2 \times$  $10^3 \,\mathrm{M}^{-1}$  for Yb<sub>2</sub>O<sub>3</sub>/TiO<sub>2</sub>. The adsorption isotherms could be fitted by a simple Langmuir equation.

The discussion henceforth pertains to the factors leading to the enhanced activity of the lanthanide oxide doped  $TiO<sub>2</sub>$  catalysts. The crystalline phase of the titania catalyst is an important factor that determines its activity. The lanthanide oxide containing catalysts exist predominantly in the anatase phase, whereas the nonmodified  $TiO<sub>2</sub>$  catalyst contains 20% of rutile phase. One possible reason for the decrease in activity of the nonmodified  $TiO<sub>2</sub>$  particles could be the presence of the rutile phase. The phase change from anatase to rutile occurs in the temperature range of 600–1100◦C. It has been suggested by Ovenstone and Yanagisawa (37) that a critical particle size is required for the anatase to rutile transformation. The critical particle size required for rutile formation is larger than the normal anatase crystallite size for a sol-produced powder. The presence of lanthanide oxide particles in the composite  $Ln<sub>2</sub>O<sub>3</sub>/TiO<sub>2</sub>$  photocatalysts prevents anatase particles from adhering together and thus a critical particle size necessary for the transformation from anatase to rutile is prevented. The significant differences obtained in the activities cannot be attributed to the differences in the phase composition alone.

Another factor that could greatly influence the photocatalytic activity is the surface area of the catalysts. The surface areas of  $Eu_2O_3/TiO_2$  and  $Pro_3/TiO_2$  are similar (102.1 m<sup>2</sup> g<sup>-1</sup> and 125.0 m<sup>2</sup> g<sup>-1</sup>, respectively) while that of  $Yb_2O_3/TiO_2$  is about 25% lower than that of  $Eu_2O_3/TiO_2$ . The surface area of the nonmodified TiO<sub>2</sub> is 78.1 m<sup>2</sup> g<sup>-1</sup>. The photocatalytic activity of  $Yb_2O_3/TiO_2$  is comparable to the other lanthanide oxide doped catalysts, suggesting that the differences in the surface area cannot be a controlling factor in influencing the photocatalytic activity.

The particles in the composite photocatalysts consist of lanthanide oxides and  $TiO<sub>2</sub>$  particles. The formation of a heterojunction between  $TiO<sub>2</sub>$  and  $Ln<sub>2</sub>O<sub>3</sub>$  could prevent electron–hole recombination and enhance the activity. However, the conduction band edges of lanthanide oxides lie at far more negative values (∼−1.8 to −3.5 V vs standard hydrogen electrode (SHE) compared to TiO<sub>2</sub>( $\sim$ -0.3 V vs SHE for anatase). Hence, electron transfer is not possible from the conduction band edge of  $TiO<sub>2</sub>$  to  $Ln<sub>2</sub>O<sub>3</sub>$  since the lanthanide oxides do not possess the appropriate potentials. Thus, the formation of such heterojunctions cannot explain the enhanced activity by  $\text{Ln}_2\text{O}_3/\text{TiO}_2$  photocatalysts.

The adsorption of salicylic acid and that of *t*-cinnamic acid were found to be ca. three times and two times higher, respectively, on the lanthanide oxide modified catalysts compared to the nonmodified  $TiO<sub>2</sub>$  catalyst. This would suggest that the equilibrium dark adsorption of the pollutant at the photocatalyst surface has an important role in determining the photocatalytic activity. The lanthanide oxide doped  $TiO<sub>2</sub>$  catalysts turned bright yellow upon immersion in salicylic acid solutions, whereas the nonmodified  $TiO<sub>2</sub>$  catalyst turned pale yellow. The supernatant solutions were, however, colorless. The development of a bright yellow color is a clear indication of the formation of Lewis acid–base complexes between the lanthanide ions and the carboxylic acid residues of the substrate. Complexes between the



**SCHEME 2.** Surface complex formed between salicylic acid and  $Ln<sub>2</sub>O<sub>3</sub>/TiO<sub>2</sub>$  catalysts.

substrates and pure  $TiO<sub>2</sub>$  can also be formed. The equilibrium constant for the formation of  $T_1^{4+}$ –salicylic acid is estimated to be  $K = 2.2 \times 10^2$  (38) and for Ln<sup>3+</sup>–salicylic acid (Ln = Eu<sup>3+</sup>, Pr<sup>3+</sup>),  $K = 5.0 \times 10^2$  (39). Thus, the relative tendency for the formation of surface complexes of the type described in Scheme 2 is higher for  $\text{Ln}^{3+}$  compared to  $Ti<sup>4+</sup>$ . The concentration of the pollutant at the photocatalyst could provide the mechanism for the enhanced mineralization by the modified catalysts. We interpret our enhanced adsorption of salicylic acid due to the formation of surface complexes as described in Scheme 2. The adsorption of *t*cinnamic acid over the lanthanide oxide doped  $TiO<sub>2</sub>$  catalysts was found to be lower when compared with salicylic acid. The lower adsorption for *t*-cinnamic acid can be explained by considering that it does not have the appropriate stereochemical configuration to make ring formation possible as in salicylic acid. Thus the behavior of *t*-cinnamic acid lends credence to our suggested structure of the surface complex.

An enhancement of the activity would also occur if the surface complex between the lanthanide ions and the organic acid is photoactive and helps in a charge transfer reaction.

The photocatalytic oxidation involves multiple steps. The identification of intermediates depends on the stability of the intermediates themselves as most of them undergo rapid oxidation. In the present work, in the case of lanthanide oxide doped  $TiO<sub>2</sub>$  catalysts, oxalic acid was detected as the *only* intermediate. The formation of oxalic acid as the only intermediate indicates the degradation route to complete mineralization of the substrates to  $CO<sub>2</sub>$ . The exact reason for the formation of only oxalic acid in solution is unclear at the moment since oxalic acid too has a tendency to bind to the lanthanide ions. In the case of the nonmodified  $TiO<sub>2</sub>$  catalyst, the photodegradation is slow and incomplete. Twenty intermediates were observed but their concentrations were too low to be quantitatively estimated.

In conclusion, we have designed a new class of photocatalysts for the degradation of functionalized aromatic acids. The photocatalysts consist of lanthanide oxide/ $TiO<sub>2</sub>$ composites. The present study has demonstrated that europium, praseodymium, and ytterbium oxide doped  $TiO<sub>2</sub>$ exhibit significantly higher activity compared to the nonmodified  $TiO<sub>2</sub>$  catalyst. The enhanced degradation by the

lanthanide oxide doped  $TiO<sub>2</sub>$  is thus general, and other organic compounds such as *p*-chlorophenoxyacetic acid, *p*-nitrobenzoic acid, and aniline can be completely mineralized. Since the photodegradation involves oxidative mineralization, the intermediates are bound to the lanthanide ions and their surface degradation prevents their appearance in solution. The loading of the lanthanide ions is also an important parameter.

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